DEVICE FOR STEEPING CEREALS

This invention relates to a container for barley to be steeped, with a floor that is provided with passageways for passing water between the underside of the floor and the barley to be steeped in the container.

As known to the expert, brewing beer requires that barley be cleaned and steeped prior to the malting process, wherein the barley grains are moved to more or less of an extent in order to germinate. Known here is the use of a so-called steeping cistern provided with a double, flat floor. The top floor of the double floor is here perforated, wherein the perforated passageways are small enough to prevent barley grains brought from above onto the top floor of the double floor from passing through these perforated passageways. The distance between the two floors of the double floor normally measures at least about 80 cm.

While the barley is cleaned and steeped in the known steeping cistern, the barley is introduced into the cistern on the top floor of the double floor. In the steeping cistern, the barley is subjected to a treatment primarily involving two alternating and repeating phases. During the first phase, the barley is supplied with water via the double floor, wherein not just the barley, but also the dual floor is submerged under the water. Also referred to as the wet steeping phase, this phase typically lasts about 2 to 5 hours. In the second phase that follows the wet steeping phase, which is also referred to as dry steeping phase, and generally lasts for about 10 hours, the water is drained from the steeping cistern, wherein the water that was above the first floor of the double floor during the wet steeping phase flows through the perforations in the top floor of the double floor.

During the steeping process, the moisture content in the (living) grains increases, thereby accelerating the conversions into the grains necessary for sustaining life. In these conversions, starch compounds are enzymatically converted in water and carbon dioxide, for which purpose oxygen is additionally needed from the environment. During the wet steeping phase, the water is aerated to supply oxygen and expel carbon dioxide. In the dry steeping phase, the air between the grains is freshened through aeration, which expels carbon dioxide and supplies oxygen.

One important objection associated with using a flat steeping cistern with a double floor is the significant level of water consumption, since the double floor is of necessity filled with water during the wet steeping phase. The typical quantities that here play a role fill the double floor with about 300 m3 of water (rule of thumb; about 0.7 m3 per m2 of steeping cistern surface), wherein about 450 m³ of water is present above the top floor of the double floor during the wet steeping phase (rule of thumb; about 1 m3 per ton of barley). There are only a limited number of options for reducing the height of the double floor is limited, since a minimum height is required to evacuate a sufficient amount of carbon dioxide from the mass of barley grains during the steeping phase. Another important objection associated with the use of known flat steeping cisterns is that cleaning it when no barley grains are present in the flat steeping distern is very time consuming and work intensive, and there is a risk that contaminants will nonetheless remain behind, an undesirable prospect given the type of end product, specifically beer.

The invention now intends to offer a solution, or at least improvement, for the set of problems described above. To this end, the device according to the invention is characterized in that a water line network under the floor is directly adjacent to passageways in order to pass water through these passageways. Using such a water line network eliminates the necessity of using a double floor, which must be filled with water during the wet steeping phase. As a result, a significant savings in water consumption can be realized.

In order to expand the functionality of the water line network, it is preferred that the water line network be set up for diverting water via the passageways starting at the barley to be steeped.

As an alternative or in combination, it is preferred that the water line network be set up for supplying water via the passageways to the barley to be steeped through the passageways starting at the underside of the floor.

To keep the water line network relatively simple in design, it is desirable to limit the number of passageways through which water is passed from or to the barley to be steeped, making it necessary to provide the passageways with a traversable surface that is significantly larger than the traversable surface of the perforation passageways in the top floor of the double floor of the flat steeping cistern according to prior art. In this case, passageways with a traversable surface of at least 50 cm², and further of at least 100 cm², are preferred. In order to now prevent barley grains from passing through these passageways, the passageways should preferably be provided with sieve units.

The container preferably has a round head shape in the top view, wherein the passageways are arranged in radially oriented rows. The advantages associated with this are primarily structural in nature.

In order to subject the barley grains in the container to the action of the water supplied through the passageways as homogeneously as possible it is preferred that the passageways be distributed over the surface of the floor in a primarily uniform fashion. This general rule might be less applicable if at all near the circumferential edge given the deviating behavior near the circumferential edges of the floor. In addition, the advantage to a uniform distribution of passageways over the surface of the floor is that, as will be explained further on, if these passageways are also used for aerating the barley grains, the barley grains can be set in motion with a minimum number of passageways, thereby generating a growing, dirt-removing and pressure-compensating effect. The barley grains will pass straight through the passageways perpendicularly upward, while a downwardly flowing stream of barley grains is obtained at some radial distance between the passageways, for example at a radial distance of between 20 and 50 centimeters, thereby yielding a more or less toroidal pattern of motion, wherein the barley grains are continuously circulated. This pattern of motion is also referred to as a recirculating effect. As already mentioned, the number of passageways must here be limited. wherein a compromise must be found between the traversable surface of the passageways, the density of passageways on the floor, and the recirculating effect. The density of the passageways on the floor is preferably less than 10, or more preferably less than 5 passageways per m2. In order to achieve the homogeneous distribution during the use of radially oriented rows as effectively as possible, even near the midpoint of

the round head shape, it is preferred that adjacent, radially oriented rows vary in length.

It is very preferred that the water line network under the floor be provided with a series of shared water line elements, and with water branch line elements, between a shared water line element and a passageway. This limits the tube length required for the water line network.

When using radially oriented rows of passageways, it is preferred that the shared water line elements be radially oriented, so that the orientation of rows, passageways and shared water line elements coincide, and the water branch line elements in between can be essentially uniform in design.

It is here further preferred that the shared water line elements be arranged between two adjacent radially oriented rows of passageways viewed from above, so that the water branch line elements can be connected right next to the passageways of the two adjacent, radially oriented rows at one end, and right next to the same shared water line element at their opposite end.

In order to also limit the tube length necessary for the water line network, it is further preferred that a number of shared water line elements be connected to a water main line element.

One important advantage in terms of the simplicity with which the device can be cleaned in the interim is achieved by providing a container for cleaning agents that is connected by a cleaning agent valve with the water line network, so that cleaning agents can be added to the water line network when desired. It must here be kept in mind that the amount of water the water line system can hold is many times less than the volume of the double floor of the flat steeping cistern according to prior art. As already mentioned, the latter volume usually measures 300 m³, while a typical volume for the inside of the water line system measures 5 m³, so that the application of a container for cleaning agents with which the so-called clean-in-place process can be performed lies within the realm of possibility. It also holds true that using a water line system inside the water

line system enables far higher flow rates, which also already yields an improved cleaning effect.

In addition, there are major advantages to directly connect a carbon dioxide line system to the passageways under the floor in order to remove carbon dioxide from the barley to be steeped via these passageways. Even though these passageways can in principle relate to passageways other than the passageways used to supply air from the water line system to the barley to be steeped (wherein the dimensions and number of passageways for the carbon dioxide and passageways for the water can deviate from each other, if needed), it is here preferred that the same passageways be used for supplying (and potentially discharging) water that were used to evacuate the carbon dioxide from the barley mass during the dry steeping phase.

In order to limit the necessary tube length for realizing the carbon dioxide line system, the latter is preferably provided under the floor with a number of shared carbon dioxide line elements and carbon dioxide branch line elements between a shared carbon dioxide line element and a passageway. The advantages to a shared carbon dioxide line element and carbon dioxide branch line element are comparable to the application of shared water line elements and water branch line elements.

From the same standpoint, it is further preferred that a number of shared carbon dioxide line elements be connected to a carbon dioxide main line element. Connecting this carbon dioxide main line element to a vacuum source can generate a reduced pressure inside the entire carbon dioxide line system to evacuate the carbon dioxide via the corresponding passageways.

An efficient use of the used line elements is achieved by having the shared water line elements and shared carbon dioxide line elements be formed at least in part by the same shared line elements.

An identical advantage comes into play when the water branch line elements and carbon dioxide branch line elements are formed at least in part by the same branch line elements. The same branch line elements

can be used for both supplying (and potentially discharging) water and removing carbon dioxide, since supplying (or discharging) water does not take place simultaneously with carbon dioxide removal.

In order to now prevent carbon dioxide from inadvertently getting into the water main line elements during the use of shared line elements, it is preferred that a water valve be provided between the shared line elements and water main line element.

For a comparable reason, namely to prevent water from penetrating into the carbon dioxide main line element, it is preferred that carbon dioxide valves be provided between the shared line elements and the carbon dioxide main line element

It is also very much preferred for an air line system to be connected to the passageways under the floor, so that air can be supplied to the barley to be steeped via these passageways. As in the case of the passageways for the carbon dioxide, it also holds true that the passageways for air (or oxygen) can in principle be passageways other than the passageways for passing through water, and hence can also deviate in terms of number and dimensions, but that the passageways intended for supplying air to the barley preferably be the same as the passageways for passing through water and/or the passageways for removing carbon dioxide.

In order to limit the tube length required for realizing the air line system, the air line system is preferably provided with a number of shared air line elements and air branch line elements between a shared air line element and a passageway. In addition, it is preferred within this framework that a number of shared air line elements be connected to an air main line element. Connecting the air main line element to a compressor or the like makes it possible to realize an elevated pressure inside the air line system in order to supply air to the barley to be steeped.

It is preferred that air valves be provided between the shared air line elements and air main line element, so that passageways can be provided in groups for air.

It is here advantageous to provide a control system suitable for the individual or group operation of various air valves.

In order to remove contaminants or the like that circulate on the water in the container, it is preferred that the container be provided near its upper side with a scraper, so that the elements circulating on the water can be scraped off while shifting the scraper in a displacement direction along the surface of the water.

To facilitate the shifting of undesired particles, such contaminants, to the surface of the water in the container, air can be supplied as a stimulus through the air supply passageways. Since the scraper is only effective directly on its front side, another preferred embodiment of the device according to the invention is characterized in that the control system is suitable for opening one or more air valves located in the displacement direction on the front side of the scraper viewed from above.

The invention will be explained in greater detail based on the description of a preferred embodiment of a steeping device according to the invention drawing reference to the following figures:

- Fig. 1 shows a perspective view of a steeping cistern (partially transparent view);
- Fig. 2 shows a detailed perspective view of part of the steeping cistern according to Fig. 1;
- Fig. 3 shows a detailed portion of Fig. 2;
- Fig. 4 shows a top view of a possible distribution pattern of passageways on the floor of the steeping cistern according to Fig. 1.

Fig. 1 shows a steeping cistern 1 for steeping barley for the malting process, e.g., for brewing bear. For example, the steeping cistern 1 can be arranged at the top on a malting tower, which is advantageous from a logistical standpoint, since the steeped barley is subjected to ensuing steps in the malting process after steeping.

The steeping cistern 1 encompasses a container in the form of a cylindrical container 2 with a perpendicular wall 3 and a flat floor 4 abutting the lower side of this perpendicular wall 3 with a diameter of 24 meters. The container 2 is meant to be filled through its open upper side with barley 5 to be steeped, and also to be filled with water during the wet steeping phase.

Located in the middle of the container 2 is a cylindrical support 27 with a central, perpendicular rotational axis 28 for a bridge 29, which extends between the support 27 and the perpendicular wall 3 of the container 2.Connected to the underside of the bridge 29 is a curved scraper body 30 provided with a scraping wall 31 located at the level of the water surface in the container 2 during the wet steeping phase. Situated in the trough of the scraper body 30 is a capstan 32 for removing material, moved by the scraper body 30 from the surface of the water in container 2 in the direction of the support 27. To this end, the support 27 is provided with passageways (not shown in greater detail) for removing the material through the inside of the support 27.

The floor 4 of the container 2 is provided with a number of passageways 6 for passing through agents like water, air/oxygen and carbon dioxide, which play a role in the steeping process. The passageways 6 are arranged in radial rows 7 (Fig. 4), which vary in length. In particular, the long rows 7a extend over nearly the entire radius of the floor 4, and the short rows 7b extend only on the outer half of the radius of the floor 4. The passageways 6 are situated among each other in every radial row 7 spaced roughly the same distance apart. The angle formed by the adjacent rows 7 with each other measures about 6 to 7 degrees. The optimal angle depends on the diameter of the floor. This yields a regular pattern of passageways 6, wherein the distribution of passageways 6 over the surface of the floor 4 is uniform. The density of the passageways 6 averages about 1 passageway per m² of floor area.

The diameter of each passageway 6 measures about 10 cm. In order to prevent barley grains from passing through the passageways 6, the later are provided with sieve material 8. The passageways 6 are formed from the upper side of a conical accumulator 9 on the inclined lateral wall, from which one air branch line 10 is connected, and to which a combined branch-on line 11 is connected centrally in the middle on the bottom side. On the side opposite the accumulator 9, the air branch line 10 connects to a shared air line 12, to which the air branch lines 10 belonging to other passageways 6 in the same series 7 and an adjacent row 7 are connected. The combined branch lines belonging to the passageways 6 of the same radial rows 7 connect to a shared combined line on their side lving opposite the accumulator 9. In the top view, the various shared air lines 12 and the various shared combined lines 13 are located between two adjacent radial rows 7. Just as the rows 7, the shared air lines 12 and the shared combined lines 13 therefore also extend in a radial direction. wherein the shared air lines 12 are located over the accompanying shared combined lines 13. The diameter of the shared combined lines 13 tapers off toward the middle, so that enough pressure can also be exerted near the middle of the floor when water is supplied to the passageways 6 via the shared combined lines 13

On the outside of the container 2, the shared air lines 12 connected to an annular air main line element 14, which is hooked up to a compressor 34 to increase the pressure inside the air line system, which consists of the air main line element 14, the shared lines 12 and the air branch lines 10. The air pressure inside the air line system can hence be increased to a pressure exceeding the static pressure owing to the water column (e.g., 0.5 bar or more) in order to supply air to the barley 5 through passageways 6. The air valves 23 between the shared air lines 12 and the air main line element 14 must be open for supplying air.

The outside of the shared combined lines 13 connect with a water main line element 15 or a CO₂ main line element 16. As with the air main line element 14, the water main line element 15 is annular, and extends all around the periphery of the container 2 on its bottom side. In the water line system comprised of the water line main line element 15, the shared combined line 13 and the combined branch line 11, water can be supplied

via the supply line 17 by opening the water valve 19 and connecting the water valve 20 to the barley 5 via passageways 6, while water can also discharged via the same water line system from the container 2 through passageways after closing the water valve 19 and opening the water valve 20 via discharge line 18. The water valves 21 between the shared combined lines 13 and the water main line element 15 must here be opened, while the CO₂ valves 22 between the shared combined lines 13 and the CO₂ main line elements 16 must be closed. The water main line element 15 is connected to a reservoir 25 via cleaning liquid valves 26. The reservoir 25 contains cleaning liquid, e.g., lye, which can be supplied to the water in the water main line element 15 with the cleaning liquid valve 26 open.

A total of four CO₂ main line elements 16 are provided, wherein each traverses a quarter circle around the periphery of the container 2. The CO₂ main line elements 16 have an increasing diameter, wherein a vacuum pump 24 is provided on the side of the largest diameter (see Fig. 1). The action of the fans 24 makes it possible to remove CO₂ from the barley via the carbon dioxide line system consisting of the four carbon dioxide main line elements 16, the shared combined lines 13 and the combined branch lines 11.

The arrangement of passageways 6 in the sieve material 8 of the floor 4 is preferably optimized via flow simulation.

The passageways 6 are arranged in rows 7 (and 7a, 7b) in the exemplary embodiment, wherein these rows are simultaneously designed as a support for the floor 4, and discharge the floor load.

The passageways 6 could also be arranged between the rows 7, however.

The CO₂ main line element 16 can be arranged as shown on Fig. 1, or closer to the floor 4 or at the upper edge of the container 2.

In addition to evacuating CO₂ from the barley 5 via the passageways 6 or accumulators 9, compressed air can also be introduced into the barley 5 via the air branch line 10. To this end, each line connection is provided

with a check valve between the air branch line 10 and accumulator 9 (not explicitly shown) to prevent water from penetrating. This improves sanitation.

Air branch lines 10 and branch-in lines 11 are preferably flexible or elastic in design.

The accumulators 9 constitute part of the floor 5, and preferably lased like the holes in the sieve jacket.

The combined lines 13 form an inlet and outlet, while the main line is only used as an inlet for the air branch lines 10.

The floor 4 and sieve material 8 in the example are designed in such a way that gridirons are arranged between the rows 7, 7a, 7b, and the floor abuts the rows 7, 7a, 7b as a perforated plate with the sieve openings.

The steeping cistern 1 functions as follows: Starting from an unfilled state of the container 2, the barley 5 is introduced into the container 2. Water is then supplied via the water line system to the barley 5 through the passageways 6, so that the barley 5 is completely immersed in the water. This state of the wet steeping phase is retained for several hours, for example two or three hours. Because the passageways 6 are arranged in radial rows 7 and separate air valves 23 that can be individually opened and closed by a control system (not shown in any greater detail) are used per row, it is possible during the wet steeping phase to selectively provide rows 7 with air during the rotation of the scraper body 30 in a rotational direction 33 directly preceding the scraper body 30 with viewed from above, so that dirt there floats up locally to more of an extent, and can be removed via the scraping wall 31 through the capstan 32.

After the steeping phase, the water is again allowed to drain from the container 2 via passageways 6 by opening the water valve 20. The barley 5 then allowed to dry to more or less of an extent during the so-called dry steeping phase. During this dry steeping phase, which lasts five hours, for example, the barley grains swell and respire faster, to which end the barley grains absorb oxygen, and the barley grains release CO₂. In order

to keep this process going, oxygen is supplied to the barley as part of the air via the oxygen line system, while the CO_2 is evacuated from the barley through fans 24 with the CO_2 valves 22 open and water valves 21 closed. The combined branch lines 11 and shared, combined lines 13 are here both used for supplying and discharging water, and for evacuating CO_2 . The wet steeping phase and dry steeping phase described above can alternate a few times until steeping has reached a sufficient level, and the steeped barley is suitable for the malting process.

For cleaning the steeping cistern 1, and above all for cleaning the water line system, this water line system can be rinsed thoroughly with water provided with cleaning liquid from the reservoir 25. The type of line system here enables the realization of relatively high flow rates for the cleaning liquid, so that cleaning can take place effectively, while the necessary quantity of cleaning liquid remains limited due to the restricted quantity relative to the water line system. The expert will know that the passageways 6 and primarily their sieve materials 8 and the floor 4 can be exposed to the action of the cleaning liquid in this way, wherein only a thin layer of cleaning liquid has to be applied to the floor 4 to this end. The cleaning efficiency can be further increased significantly by aerating the cleaning liquid, which imparts motion to the cleaning liquid.

REFERENCE LIST

1	Steeping cistern	17	Supply line
2	Container	18	Discharge line
3	Wall	19	Water valve
4	Floor	20	Water valve
5	Barley	21	Water valve
6	Passageway	22	CO2 valve
7	Row	23	Air valve
7a	Long row	24	Vacuum pump
7b	Short row	25	Reservoir
8	Sieve material	26	Cleaning liquid valve
9	Accumulator	27	Support
10	Air branch line	28	Rotational axis
11	Branch-in line	29	Bridge
12	Air line	30	Scraper body
13	Combined line	31	Scraping wall
14	Air main line element	32	Capstan
15	Water main line element	33	Rotational direction
16	CO2 main line element		